

U.S. Application No.
Unknown

International Application No.
PCT/NZ99/00084

Attorney Docket No.
DAIRY64.001APC

09/720041

Date: December 14, 2000

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**TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US)
CONCERNING A FILING UNDER 35 USC 371**

International Application No.: PCT/NZ99/00084
International Filing Date: June 14, 1999
Priority Date Claimed: June 17, 1998 (NZ Patent Application No. 330710)
Title of Invention: BIOACTIVE WHEY PROTEIN HYDROLYSATE
Applicant(s) for DO/EO/US: Ralf-Christian Schlothauer
Linda May Schollum
Anne Maria Singh
Julian Robert Reid

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. (X) This is a **FIRST** submission of items concerning a filing under 35 USC 371.
2. () This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 USC 371.
3. (X) This express request to begin national examination procedures (35 USC 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 USC 371(b) and PCT Articles 22 and 39(1).
4. (X) A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5. (X) A copy of the International Application as filed (35 USC 371(c)(2))
 - a) () is transmitted herewith (required only if not transmitted by the International Bureau).
 - b) (X) has been transmitted by the International Bureau.
 - c) () is not required, as the application was filed in the United States Receiving Office (RO/US).
6. () A translation of the International Application into English (35 USC 371(c)(2)).
7. (X) Amendments to the claims of the International Application under PCT Article 19 (35 USC 371(c)(3))
 - a) () are transmitted herewith (required only if not transmitted by the International Bureau).
 - b) () have been transmitted by the International Bureau.
 - c) () have not been made; however, the time limit for making such amendments has NOT expired.
 - d) (X) have not been made and will not be made.
8. () A translation of the amendments to the claims under PCT Article 19 (35 USC 371(c)(3)).
9. () An oath or declaration of the inventor(s) (35 USC 371(c)(4)).
10. (X) A copy of the International Preliminary Examination Report with any annexes thereto, such as any amendments made under PCT Article 34.

Date: December 14, 2000

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11. ☐ A translation of the annexes, such as any amendments made under PCT Article 34, to the International Preliminary Examination Report under PCT Article 36 (35 USC 371(c)(5)).

Items 12. to 27. below concern other document(s) or information included:

12. ☐ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
13. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
14. ☒ A FIRST preliminary amendment.
☐ A SECOND or SUBSEQUENT preliminary amendment.
15. ☒ Drawings in 3 pages
16. ☒ A power of attorney and/or address letter.
17. ☒ International Application as published.
18. ☐ Small Entity Statement.
19. ☒ PCT Form PCT/IPEA/408. (Written Opinion).
20. ☐ PCT Form PCT/IB/308.
21. ☒ PCT request form.
22. ☒ Other Items or information: Certificate of Mailing by Express Mail
23. ☒ A return prepaid postcard.
24. ☒ The following fees are submitted:

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Unknown

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526 Rec'd PCT/PTO 09/720041
14 DEC 2000
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				FEES
BASIC FEE				\$860
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE	
Total Claims	31 - 20 =	11×	\$18	\$198
Independent Claims	2- 3 =	0×	\$80	\$0
Multiple dependent claims(s) (if applicable)			\$270	\$0
TOTAL OF ABOVE CALCULATIONS				\$1,058.00
Reduction by 1/2 for filing by small entity (if applicable). Verified Small Entity statement must also be filed. (NOTE 37 CFR 1.9, 1.27, 1.28)				\$
TOTAL NATIONAL FEE				\$1,058.00
TOTAL FEES ENCLOSED				\$1,058.00
amount to be refunded:				\$
amount to be charged:				\$

25. (X) The fee for later submission of the signed oath or declaration set forth in 37 CFR 1.492(e) will be paid upon submission of the declaration.
26. (X) A check in the amount of \$1,058.00 to cover the above fees is enclosed.
27. (X) The Commissioner is hereby authorized to charge only those additional fees which may be required, now or in the future, to avoid abandonment of the application, or credit any overpayment to Deposit Account No. 11-1410. A duplicate copy of this sheet is enclosed.

NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.

SEND ALL CORRESPONDENCE TO:


KNOBBE, MARTENS, OLSON & BEAR, LLP
620 Newport Center Drive
Sixteenth Floor
Newport Beach, CA 92660

Signature

Ginger R. Dreger
Printed Name

33,055
Registration Number

PATENT

October 5, 2001
(Date)

Ginger R. Dreger, Reg. No. 33,055

Ginger R. Dreger, Reg. No. 33,055

-1-

Appl. No. : 09/720,041
 Filed : April 2, 2001

Please replace the table on page 16 with the following new table:

TABLE 3: ACE-I Peptides and their Activities

Peptide Sequence ^a	Origin	Activity ^b (IC ₅₀ in mg L ⁻¹)	Similarity to known ACE-I Peptides
AFE (Ala-Phe-Glu)	PP ^D 3(129-131)	20	
LFSH (Leu-Phe-Ser-His) (SEQ ID NO: 1)	PP3(125-128)	30	
ILKEKH (Ile-Leu-Lys-Glu-Lys-His) (SEQ ID NO: 2)	PP3(71-76)	20	
LIVTQ (Leu-Ile-Val-Thr-Gln) (SEQ ID NO: 3)	β -LG ^c (1-5)	17	
MKG (Met-Lys-Gly)	β -LG(7-9)	24	
LDIQK ^c (Leu-Asp-Ile-Gln-Lys) (SEQ ID NO: 4)	β -LG(10-14)	17	β -LG (9-14)
VF (Val-Phe)	β -LG(81-82)	19	
ALPMH (Ala-Leu-Pro-Met-His) (SEQ ID NO: 5)	β -LG(142-146)	12	β -LG (142-148)
VTSTAV (Val-Thr-Ser-Thr-Ala-Val) (SEQ ID NO: 6)	GMP ^f (59-64)	30	
LHLPLP (Leu-His-Leu-Pro-Leu-Pro) (SEQ ID NO: 7)	β -CN ^g (133-138)	7	
LVYPFPGPIPNLQNP (Leu-Val-Tyr-Pro-Phe-Pro-Gly-Pro-Ile-Pro-Asn-Ser-Leu-Pro-Gln-Asn-Ile-Pro-Pro) (SEQ ID NO: 8)	β -CN (58-76)	19	β -CN(74-76)
LFRQ (Leu-Phe-Arg-Glu) (SEQ ID NO: 9)	α_{s1} -CN(136-139)	17 ^h	

Appl. No. : 09/720,041
Filed : April 2, 2001

In the Claims:

Please amend claims 19, 26, and 29 to read as follows:

Claim 19. (Once amended) A process as claimed in claim 6 or in any claim dependent from claim 6 wherein one or more of the bioactive peptides in the resulting hydrolysate is selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEY (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYPPFGPIPNLQNP (SEQ ID NO: 8) and LFRQ (SEQ ID NO: 9).

Claim 26. (Once amended) A product as claimed in any one of claims 20 to 25 wherein one or more of the bioactive peptides is selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEKH (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYPPFGPIPNLQNP (SEQ ID NO: 8) and LFRQ (SEQ ID NO: 9).

Claim 29. (Once amended) Any one or any combination of two or more of the bioactive peptides selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEKH (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYPPFGPIPNLQNP (SEQ ID NO: 8) and LFRQ (SEQ ID NO: 9).

REMARKS

The specification and claims have been amended to include references to the SEQ ID NOs. where the sequences appear.

Attached hereto is a marked-up version of the changes made to the specification and claims by the current amendment. The attached page is captioned "Version with markings to show changes made."

Appl. No. : 09/720,041
Filed : April 2, 2001

Although no fees are believed to be due at this time, please charge any fees, including any fees for extension of time, or credit overpayment to Deposit Account No. 11-1410.

Respectfully submitted,

KNOBBE, MARTENS, OLSON & BEAR, LLP

Dated: October 5, 2001

By: 

Ginger R. Dreger
Registration No. 33,055
Attorney of Record
620 Newport Center Drive
Sixteenth Floor
Newport Beach, CA 92660
(415) 954-4114

Appl. No. : 09/720,041
Filed : April 2, 2001

In the Specification:

Please replace the paragraph beginning at page 4, line 33, with the following rewritten paragraph:

--In another embodiment the invention consists in a whey protein hydrolysate containing one or more bioactive peptides selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEKH (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYPPGPIPNQLPQNIPP (SEQ ID NO: 8), and LFRQ (SEQ ID NO: 9)--

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VF (Val-Phe)	β-LG(81-82)	19	
ALPMH (Ala-Leu-Pro-Met-His) (SEQ ID NO: 5)	β-LG(142-146)	12	β-LG (142-148)
VTSTAV (Val-Thr-Ser-Thr-Ala-Val) (SEQ ID NO: 6)	GMP ^f (59-64)	30	
LHLPLP	β-CN ^g (133-138)	7	

Appl. No. : 09/720,041
Filed : April 2, 2001

(Leu-His-Leu-Pro-Leu-Pro) (SEQ ID NO: 7)			
LVYFPFGPIPNLSLPQNIPP (Leu-Val-Tyr-Pro-Phe-Pro- Gly-Pro-Ile-Pro-Asn-Ser- Leu-Pro-Gln-Asn-Ile-Pro- Pro) (SEQ ID NO: 8)	β -CN (58-76)	19	β -CN(74-76)
LFRQ (Leu-Phe-Arg-Glu) (SEQ ID NO: 9)	α_{s1} -CN(136-139)	17 ^h	

In the Claims:

Claims 19, 26, and 29 have been amended as follows:

Claim 19. (Once amended) A process as claimed in claim 6 or in any claim dependent from claim 6 wherein one or more of the bioactive peptides in the resulting hydrolysate is selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEY (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYFPFGPIPNLSLPQNIPP (SEQ ID NO: 8) and LFRQ (SEQ ID NO: 9).

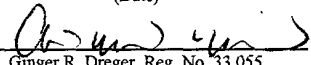
Claim 26. (Once amended) A product as claimed in any one of claims 20 to 25 wherein one or more of the bioactive peptides is selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEKH (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYFPFGPIPNLSLPQNIPP (SEQ ID NO: 8) and LFRQ (SEQ ID NO: 9).

Claim 29. (Once amended) Any one or any combination of two or more of the bioactive peptides selected from the group consisting of AFE, LFSH (SEQ ID NO: 1), ILKEKH (SEQ ID NO: 2), LIVTQ (SEQ ID NO: 3), MKG, LDIQK (SEQ ID NO: 4), VF, ALPMH (SEQ ID NO: 5), VTSTAV (SEQ ID NO: 6), LHLPLP (SEQ ID NO: 7), LVYFPFGPIPNLSLPQNIPP (SEQ ID NO: 8) and LFRQ (SEQ ID NO: 9).

DAIRY.64.001APC

PATENT

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant	:	Schlothauer, et al.)	Group Art Unit Unknown
)	
Appl. No.	:	Unknown (based on PCT Application No. PCT/NZ99/00084))	I hereby certify that this correspondence and all marked attachments are being deposited with the United States Postal Service as first-class mail in an envelope addressed to: Assistant Commissioner for Patents, Washington, D.C. 20231, on
)	
Filed	:	Herewith)	December 14, 2000 (Date)
)	
For	:	BIOACTIVE WHEY PROTEIN HYDROLYSATE)	 Ginger R. Dreger, Reg. No. 33,055
)	
Examiner	:	Unknown		

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents
Washington, D.C. 20231

Dear Sir:

The present Preliminary Amended is filed concurrently with the filing of the above-identified patent application under 35 U.S.C. §371 with the United States Designated/Elected Office (DO/EO/US). The following amendments are based on Claims 1-32 of the above-identified International Application as originally filed.

Kindly amend this application in the following aspects.

In the Claims:

Please cancel claims 2, 3, 6, 8-13, and 28, without prejudice.

Please amend the remaining claims as follows:

1. (Amended) A process for preparing a whey protein hydrolysate containing bioactive peptides which comprises [the following steps]:
 - (i) [treating] hydrolysing a whey protein-containing substrate with at least one [or more enzymes capable of hydrolysing whey proteins, to produce a whey protein hydrolysate containing bioactive peptides] heat labile protease, at a temperature of between about 30 °C and

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Filed : **Herewith**

70 °C at a pH of about 6 to about 8.5 when said protease is a neutral protease, and at a pH of about 3.5 to about 5 when said protease is an acid protease; and

(ii) terminating [the] said hydrolysis [before substantial production of unacceptable bitter flavours] when a degree of hydrolysis of no greater than 15% has been reached by deactivating said protease under conditions sufficiently mild to avoid substantial denaturation of peptides in said hydrolysate.

4. (Amended) A process as claimed in [any one of claims 1 to 3] claim 1 wherein [the] said substrate is sweet whey or sweet whey protein concentrate.

5. (Amended) A process as claimed in [any one of claims 1 to 4] claim 1 wherein the [enzyme capable of hydrolysing the whey proteins] protease is selected from the group consisting of Protease P6, Protease A, Protease M, Peptidase, Neutrase, Validase and AFP 2000 (all as herein defined).

7. (Amended) A process as claimed in claim 1 [5 or claim 6] wherein [the] said hydrolysis [is terminated by high temperature short duration heat treatment] terminating step comprises heat deactivation.

14. (Amended) A process as claimed in [any one of the preceding claims] claim 1 wherein the substrate also contains lactose, in an amount of about 5% by weight or higher.

15. (Amended) A process as claimed in [any one of the preceding claims] claim 1 wherein said lactose content is about 10% by weight or higher.

16. (Amended) A process as claimed in claim 14 [or 15] wherein the amount of lactose present in the substrate is up to about 30% by weight.

17. (Amended) A process as claimed in [any one of claims 14 to 16] claim 14 wherein the amount of lactose present in the substrate is up to about 50% by weight.

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Filed : **Herewith**

18. (Amended) A process as claimed in [any one of claims 14 to 17] claim 14, wherein the substrate is also treated with lactase and/or β -galactosidase, either before, during or after the whey protein hydrolysis, to hydrolyse the lactose to galactose and glucose and synthesize galacto-oligosaccharides.

19. (Amended) A process as claimed in claim 1 [6 or in any claim dependent from claim 6] wherein the hydrolysate so prepared contains one or more of the bioactive peptides [in the resulting hydrolysate is] selected from the group consisting of AFE, LFSH, ILKEKH, LIVTQ, MKG, LDIQK, VF, ALPMH, VTSTAV, LHLPLP, LVYPFPGPIPNSLPQNIPP and LFRQ.

20. (Amended) A non-bitter soluble [product produced by partial hydrolysis of a substrate containing whey proteins, wherein the product contains bioactive peptides and has a degree of hydrolysis of the whey proteins of below about 10%] whey protein hydrolysate produced by a process according to claim 1.

22. (Amended) A product as claimed in [either of claims 20 or 21] claim 20 wherein the mean particle size of the whey proteins in the product is less than about 30 microns.

24. (Amended) A product as claimed in [any one of claims 20 to 23] claim 20 which is substantially white in appearance.

25. (Amended) A product as claimed in [any one of claims 20 to 24] claim 20 which also contains galactooligosaccharides.

26. (Amended) A product as claimed in [any one of claims 20 to 25] claim 20 wherein one or more of [the] said bioactive peptides is selected from the group consisting of AFE, LFSH, ILKEKH, LIVTQ, MKG, LDIQK, VF, ALPMH, VTSTAV, LHLPLP, LVYPFPGPIPNSLPQNIPP and LFRQ.

27. (Amended) A food product [comprising a product] containing a whey protein hydrolysate as claimed in [any one of claims 20 to 26] claim 20.

30. (Amended) A method of reducing systolic blood pressure in a subject which comprises administering to that subject an effective amount of a product as claimed in [any one of claims 20 to 29] claim 20.

31. (Amended) A method [as claimed in claim 30] of reducing systolic blood pressure in a subject which comprises administering an effective amount of a product according to claim 26.

32. (Amended) A method [as claimed in claim 30] of reducing systolic blood pressure in a subject which comprises administering an effective amount of a peptide or a combination of peptides as claimed in claim 29.

Please add the following new claims:

--33. A process according to claim 7 wherein said heat deactivation comprises heating said hydrolysate for up to ten seconds to a temperature up to 95 °C.

34. A process according to claim 7 wherein said hydrolysis is conducted at a temperature of below 65 °C, wherein said heat deactivating step is conducted at 65 °C to 70 °C for from 10 seconds to 15 minutes.

35. A process according to claim 7 wherein said hydrolysis is conducted at a temperature below 60 °C, wherein said heat deactivating step is conducted at 60 °C to 65 °C for from 10 seconds up to 30 minutes.

36. A process as claimed in claim 1 wherein said hydrolysis terminating step comprises altering the pH of said whey protein-containing substrate to a pH at which said protease is not active.

37. A process as claimed in claim 36 wherein said hydrolysis terminating step includes heat deactivation.

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Filed : Herewith

38. A process as claimed in claim 1 wherein said hydrolysis terminating step comprises subjecting said hydrolysate to ultrafiltration with an ultrafiltration membrane having a nominal molecular weight cutoff in the range of 10-500 kDa.

39. A process as claimed in claim 1 wherein said enzyme is immobilized on an inert support during said hydrolysis step.

40. A process as claimed in claim 39 wherein said inert support is Roehn Eupergit, carrageenan particles, chitosan particles or any other suitable inert support material.

41. A process as claimed in claim 1 wherein the degree of hydrolysis is about 3-5%. --

Please charge any additional fees, including any fees for additional extension of time, or credit overpayment to Deposit Account No. 11-1410. A duplicate copy of this sheet is enclosed.

Respectfully submitted,

KNOBBE, MARTENS, OLSON & BEAR, LLP

Dated: December 14, 2000

By: [Signature]
Ginger R. Dreger
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Sixteenth Floor
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BIOACTIVE WHEY PROTEIN HYDROLYSATE**TECHNICAL FIELD**

5 This invention relates to a process for producing hydrolysed whey protein products which are free of bitter flavours and which contain bioactive peptides. The products of the process have high digestibility and good organoleptic properties. The products may have either a bland or slightly sweet taste and are free of soapy or brothy flavours. The hydrolysed whey protein products may optionally contain oligosaccharides and are
10 useful sources of bioactive peptides for incorporation into functional foods.

BACKGROUND ART

A number of food ingredients and foodstuffs have been produced from the hydrolysis
15 of a protein source such as the milk proteins, casein and whey proteins.

Hydrolysed protein foodstuffs may have advantages over non-hydrolysed protein foodstuffs in a number of areas of health care. For example, it is known that enzymatically hydrolysed proteins are less allergenic. They are also more rapidly
20 digested and absorbed than whole proteins. Foodstuffs containing hydrolysed proteins are also useful in the alimentation of hospital patients with digestive diseases for example.

Hydrolysis of whey proteins and caseins is known to release bioactive peptides that can
25 exhibit a number of physiological effects (Maubois et al, 1991; EP 475506). A number of publications describe such bioactive peptides, for example, ACE inhibiting peptides which have antihypertensive properties have been released through an enzymatic treatment of bovine β -lactoglobulin and whey protein concentrates (Mullally et al, 1997). ACE inhibitory peptides are also found in sour milk and in hydrolysates of α_s and β
30 casein (JP 4282400; Nakamura et al 1994, Yamamoto et al 1994).

EP 4745506 discloses the hydrolysis of the milk protein lactoferrin in whey to release lactoferricin which acts as an antimicrobial agent useful for treating diarrhoea, athlete's foot, eye infections, mastitis etc in humans and animals.

35

However, the hydrolysis of most food proteins, especially the hydrolysis of whey and casein containing products, is known to generate bitterness. This causes palatability

problems particularly when attempting to formulate orally ingestible products incorporating milk protein hydrolysates as a source of bioactive peptides.

In the field of protein hydrolysis one or both of two approaches are commonly used for
5 controlling or removing bitterness in protein hydrolysates to increase palatability of the products.

The extensive hydrolysis of the protein substrate is known to reduce bitterness in milk protein hydrolysates (EP 065663; EP 117047; US 3970520). Less bitter products are
10 produced relatively easily and cheaply in this way. However, extensive hydrolysis reduces the chain lengths of all peptides, including the bioactive peptides of interest. Extensive hydrolysis of the protein substrate destroys the functional and biological activity of the peptide of interest. In addition soapy and brothy off-flavours often develop, with the consequence that the palatability of the final product remains poor
15 compared to the original bland tasting protein substrate. A final disadvantage is that for some hydrolysates the bitterness is only partially removed (Roy 1992 and 1997).

A second common method for the control of bitterness in protein hydrolysates is to use debittering enzymes, in particular those sourced from *Aspergillus oryzae*.
20

"Bitterness" generation in protein hydrolysis is thought to be due to the presence of large hydrophobic 'bitter' peptides. Debittering enzymes selectively hydrolyse bitter peptides present in the protein hydrolysates. A worker skilled in the art can - by the judicious selection of debittering enzymes and the conditions of treatment - effectively debitter
25 milk protein hydrolysates leaving intact the particular bioactive peptides of interest. However, use of debittering enzymes makes the process more expensive, and preservation of some of the bioactive peptide is not easily or successfully achieved. A further disadvantage is that debittering enzymes treatments have a tendency to release free amino acids into the final product and, as a consequence, the hydrolysates develop
30 unpleasant brothy or soapy flavours (Roy 1992 and 1997).

The various methods of debittering the protein hydrolysates result in additional process steps and add costs to the manufacture of the final product. In addition the final product also becomes overbalanced in its supply of free amino acids.
35

It would be most advantageous if a process for hydrolysing protein could be developed which releases bioactive peptides of interest and which limits the formation of bitter

peptides and free amino acids, thereby allowing the original bland taste of the milk proteins substrates to be retained.

Some bioactive peptides - in particular the antihypertensive peptides - are relatively
5 stable during protein hydrolysis and are released very early during the hydrolysis of the milk protein substrate as shown in Figure 1.

The bitter flavours of milk protein hydrolysates can be improved by adding sugars or by hydrolysing natural sugars, such as lactose, already present in the milk protein substrate
10 (Bernal and Jelen, 1989). For example sour wheys and cheese wheys are made more palatable when they have been sweetened by β -galactosidase and lactase hydrolysis of lactose (FR 2309154; US 4358464; JP 8056568).

In order to achieve a high flavour acceptability for a hydrolysed protein product which
15 contains bioactive peptides, precise control of hydrolysis is required to prevent bitterness occurring.

A common method of termination of hydrolysis is by deactivation of the enzymes, usually by thermal deactivation at high temperatures, typically > 90-100°C for an
20 extended period of time. However, this method cannot be used to stop the hydrolysis of whey proteins as any intact unhydrolysed whey proteins remaining in the mixture would denature and precipitate making the final product less soluble and less acceptable for the use as a food ingredient.

25 It would be advantageous if a process of hydrolysing whey protein could be controlled so that it directly produced a hydrolysate comprising bioactive peptides for incorporation into functional foods which did not taste bitter and where the enzyme inactivation steps did not compromise the integrity of the intact proteins in the final product.

30

It is an object of the invention to go some way towards achieving these desiderata or at least to offer the public a useful choice.

SUMMARY OF THE INVENTION

35

Accordingly the invention may be said broadly to consist in a process for preparing a whey protein hydrolysate containing bioactive peptides comprising hydrolysing a whey protein-containing substrate with one or more enzymes characterised in that:

- 5
- i) the enzyme is a heat labile protease,
 - ii) the hydrolysis is conducted at a temperature of between about 30°C and 70°C at a pH of about 6 to about 8.5 when said enzyme is a neutral protease, and at a pH of about 3.5 to about 5.0 where said enzyme is an acid protease,
 - iii) the hydrolysis is terminated when a degree of hydrolysis of no greater than 15% has been reached,
 - iv) the hydrolysis is terminated by deactivating said one or more enzymes, and
 - 10 v) the conditions for said step iv) are sufficiently mild to avoid substantial denaturation peptides or residual proteins in said hydrolysate.

Preferably said substrate is sweet whey or sweet whey protein concentrate.

15 Preferably the enzyme is selected from the group consisting of Protease P6, Protease A, Protease M, Peptidase, Neutrase, Validase and AFP 2000.

Preferably said enzyme deactivating step iv) comprises heat deactivation.

20 Preferably said heat deactivation comprises heating said hydrolysate for up to ten seconds to a temperature up to 95°C.

Preferably said hydrolysis has been conducted at a temperature of below 65°C, and said heat deactivating step is conducted at 65°C to 70°C for from 10 seconds to 15 minutes.

25 Preferably said hydrolysis has been conducted at a temperature below 60°C, and said heat deactivating step is conducted at 60° to 65°C for from 10 seconds up to 30 minutes.

Preferably said enzyme deactivating step comprises altering the pH of said whey protein-containing substrate to a pH at which said protease is not active.

30 Preferably said enzyme deactivating step includes heat deactivation as defined above.

Alternatively said enzyme deactivating step iv) comprises subjecting said hydrolysate to ultrafiltration with an ultrafiltration membrane having a nominal molecular weight cutoff
35 in the range of 10-500kDa.

Alternatively said enzyme is immobilised on an inert support during said hydrolysis step ii).

Preferably said inert support is Roehn Eupergit, carrageenan particles, chitosan particles or any other suitable inert support material.

Preferably the degree of hydrolysis is from about 3% to about 5%.

Preferably the substrate also contains lactose, in an amount of up to 50% by weight.

10

Alternatively, the substrate also contains lactose in an amount of up to 30% by weight.

Preferably the substrate is also treated with lactase and/or β -galactosidase, either before or during the whey protein hydrolysis, to hydrolyse the lactose to galactose and glucose and synthesize galacto-oligosaccharides.

In another embodiment the invention consists in a whey protein hydrolysate containing one or more bioactive peptides selected from the group consisting of AFE, LFSH, ILKEKH, LIVTQ, MKG, LDIQK, VF, ALPMH, VTSTAV, LHLPLP, LVYFPFGPIPNQLPQNIPP and LFRQ.

20

The enzyme hydrolysis step may be carried out under conditions which are suitable for the particular enzyme used as would be understood by a person skilled in the art.

The whey protein substrates are hydrolysed at a concentration in the range from 5-50% solids and the enzyme or enzyme mixtures are added to give an enzyme to substrate ratio between 0.01% and 3% w/w total solids, preferably between 0.01% and 1.0% w/w total solids.

Protein substrates treated with acid proteases may be hydrolysed at pH between 2.5 and 6.0, preferably between pH 3.0 and 5.0.

Protein substrates treated with neutral proteases may be hydrolysed at pH between 3.5 and 9.0, preferably between pH 6.0 and 8.0.

35

Protein substrates treated with alkaline proteases may be hydrolysed at pH range between 5 and 10.0, preferably between pH 6.0 and 8.0.

The protein hydrolysis may be carried out at a temperature range of from 30-65°C, preferably from 50-60°C.

The hydrolysis of lactose may be carried out at a prior stage to the whey protein hydrolysis, concurrently therewith or subsequently. The enzymes used for lactose hydrolysis may comprise lactase and/or β -galactosidase and may be selected from yeast or fungal sources eg *Kluyveromyces lactis*, *Saccharomyces lactis*, *Saccharomyces fragilis*, eg *Aspergillus niger*, *Aspergillus oryzae* such as Maxilact (Gist Brocades) and Novolact (Novo Nordisk). The lactose hydrolysis is carried out under conditions which would be known to persons skilled in the art.

In one embodiment termination of the hydrolysis is achieved by deactivating the one or more whey protein hydrolysis enzymes (and/or the lactose hydrolysing enzymes added previously) by firstly changing the pH of the reaction mixture to a pH in which the enzyme(s) is either inactive or less active, and/or heating the reaction mixture to a comparatively mild temperature using a heat exchanger to denature the enzyme but not the intact whey proteins in the substrate. A suitable temperature range which would denature the enzymes is in the order of 55-70°C, preferable 65°C.

According to one option, depending on the enzyme(s) used, the enzyme or enzyme mixture may also be deactivated by the evaporation and drying procedures.

According to another option the enzyme or enzyme mixture may also be deactivated with or without a prior pH change.

Alternatively, the one or more enzymes used to selectively hydrolyse the whey protein may be immobilised on an inert support such as Rochm Eupergit, Carrageenan particles, chitosan particles or any other suitable material and then used in a stirred tank or fixed bed reactor or on a membrane or on a hollow fiber reactor.

Alternatively, the enzyme(s) to be used for the hydrolysis could be cross linked to suitable inert support prior to the hydrolysis reaction and subsequently separated out of the hydrolysis reaction with the use of a microfiltration membrane.

Alternatively, the enzyme can be separated away from the hydrolysis mixture with the use of an ultrafiltration membrane with a nominal molecular weight cutoff in the range 10 - 500 kDa once hydrolysis is complete.

After hydrolysis and optional deactivation or removal of enzymes, the hydrolysate may optionally be subjected to reverse osmosis under conditions whereby salt and water are removed from the hydrolysate. The purified desalted hydrolysate comprising whey proteins and bioactive peptides is then recovered. If lactose hydrolysis is also chosen
5 then the hydrolysate will also contain glucose, galactose and/or galacto-oligosaccharides.

Optionally the hydrolysed whey proteins containing the bioactive peptide fraction can be separated with a UF membrane of 5-200 kDa cut off, preferably 10-50 kDa cut off.

The bioactive peptides, other peptides and, optionally, hydrolysed lactose is recovered
10 in the permeate.

According to another option ion exchange or hydrophobic adsorption or hydrophobic interaction chromatography or combinations of these processes may be used to recover the hydrolysed bioactive fraction from the hydrolysates in an enriched form.

15 In addition, lactase and β -galactosidase hydrolysis of lactose produces galacto-oligosaccharides which are known to stimulate the growth of beneficial gut flora thereby adding to the bioactive properties of the hydrolysates.

20 Hydrolysates which have been treated to further hydrolyse lactose are useful as food additives for consumers who are lactose intolerant.

The hydrolysed whey protein product of the invention has one or more of the following features:

- 25 • antihypertensive ACE-I activity
• bifidus growth promoting activity
• non-glucy, non-bitter flavour
• pleasant to slightly sweet taste
• good organoleptic properties.

30 The invention consists in the foregoing and also envisages constructions of which the following gives examples.

BRIEF DESCRIPTION OF THE DRAWINGS

35 The present invention will now be described with reference to the accompanying drawings in which:

Figure 1 is a plot of bitterness and bioactivity on the ordinant against the degree of hydrolysis on the abscissa. The 'opportunity window' of obtaining a product according to the present invention containing bioactive peptides and having acceptable flavours before the hydrolysis reaction produces bitter peptides is between the lines x_1 and x_2 .

Figure 2 is a plot of systolic blood pressure of four groups of hypertensive rats fed different diets over a period of eight weeks.

Figure 3 is a plot of a least squares means analysis of rats fed with a control of commercial rat chow against groups of rats fed with hydrolysate at two different concentrations per day.

DETAILED DESCRIPTION OF THE INVENTION

As discussed above, the present invention provides a process for producing a hydrolysed whey protein product containing bioactive peptides, whereby the hydrolysis is carried out under a high degree of control to prevent undesirable flavours developing during hydrolysis (eg bitter, soapy and brothy). The hydrolysis is terminated within the "opportunity window", ie before the emergence of substantial bitterness - as shown in Figure 1 - to provide hydrolysates having good organoleptic properties and maximum bioactive peptides. In Figure 1 the degree of hydrolysis is represented qualitatively on the x axis. The window of opportunity is between the points x_1 and x_2 which will vary depending on the enzyme which is used. The optimum conditions sought are a maximum bioactivity with an acceptable level of bitterness.

In particularly preferred embodiments of the process of the invention, the enzyme which hydrolyses the whey proteins is selected from the group consisting of Protease P6, Protease A, Protease M, Peptidase, Neutrase, Validase and AFP 2000 (all as herein defined) and the hydrolysis of the whey proteins is terminated by heat treatment for a short time at a high temperature (about 85-100°C for 1-10 seconds). The applicants have surprisingly found that the above enzymes (1) are able to produce a whey protein hydrolysate containing a good level of bioactive peptides, and (2) can be inactivated by a short time, high temperature treatment which causes only partial denaturation of the whey proteins in the hydrolysate, and surprisingly improves the organoleptic properties of the whey proteins, in terms of providing a product which is creamy in texture (has a relatively small particle size) and substantially white in appearance.

The present invention is now exemplified by the following examples:

Example 1

5 A 10% solution of a sweet whey protein concentrate with 80% protein content (ALACEN™ 392, 2L) was hydrolysed at 50°C with the commercially available enzyme Neutrase sourced from *Bacillus subtilis* (Novo Nordisk, Denmark). A pH of 7.0 and an enzyme substrate ratio of 0.3% w/w was used for the hydrolysis. The hydrolysate was adjusted to pH 5.0 and heated at 65°C for 30min to inactivate the enzyme. The
10 hydrolysate (DH of 4.5%) was spray dried and tested for angiotensin-converting enzyme inhibitor (ACE-I) activity and flavour. ACE-I activity in the dried product was determined using FAPGG as a substrate (Product 305-10 ex Sigma Chemical Corporation, St Louis, MO, USA) according of the method of D W Cushman & H S Cheung (1971). ACE-I activities are expressed as the amount of material (g/L) needed
15 to reduce the activity of the ACE-I enzyme by 50%. IC₅₀ ACE-I activity in the hydrolysate was 0.44g/L and flavour acceptability score, as determined by a taste panel, was very high.

Example 2

20 A 50% solution of ALACEN™ 421 whey protein concentrate (56% protein content, 10L) was treated with commercial lactase sourced from *Kluyveromyces lactis* (Lactozyme 3000L ex Novo Nordisk) at an enzyme to substrate ratio of 0.3% at 50°C for 2 hours. The lactase treated solution was hydrolysed with Neutrase (Novo Nordisk, Denmark) for
25 1 hour at 50°C at an enzyme substrate ratio of 0.3%. Active enzymes were inactivated by UHT treatment (5sec at 95°C) after a five fold dilution of the mixture. The hydrolysate was spray dried. The dry powder (DH 2.8%) contained no traces of active enzyme and had an ACE-I activity of 2.18g/L. The flavour score was exceptionally high due to the introduction of a low level of sweetening into the product. ACE-I
30 measurements and flavour acceptability scoring were determined as for Example 1.

Example 3

A 500L hydrolysate, made from ALACEN™ 392 in a similar way to that in example 1,
35 was cooled to 10°C after enzyme inactivation. A sub-sample of the original hydrolysate was dried. The remaining hydrolysate was subjected to ultrafiltration at 10°C with a 10,000 dalton nominal molecular weight cutoff membrane (HFK 131, Koch Membrane Systems, USA). The hydrolysate (at a DH between 3.8% and 4.2%) was concentrated to

a VCF 10 and the retentate was dried directly. The permeate was concentrated by evaporation to approx 25% solids and dried. ACE-I measurement and flavour acceptability scoring were determined as for Example 1. The ACE-I activity was enriched in the permeate powder (IC_{50} of the permeate powder was 0.15g/L). ACE-I activity in the sub-sample of the dried hydrolysate before ultrafiltration was 0.43g/L. The flavour acceptability scores on the retentate powder and the spray dried powder of the feed were both high.

Example 4

10

Three different solutions from ALACENTM 392, ALACENTM 421 and a mixture of ALACENTM 392 and lactose were made up at 15% solids to yield 150 L. The solution was treated with a commercial protease from *Bacillus subtilis* Neutrase (Novo, Nordisk Denmark) and a commercial lactase from *Klyvermyces lactis* (Lactozyme 3000L ex Novo Nordisk). The addition rate of enzyme was 0.3% w/w (on protein basis) for Neutrase and 1.2% w/w (on lactase basis) for Lactozyme. The reaction continued for 2h at 50°C at a pH of 7.0. Samples of 35L were taken every 0.5h inactivated at 88°C for 3 seconds and subsequently spray dried. The ACE-I activity as specified in example 1 yielded 0.424g/L, 0.336g/L and 0.432g/L for the three mixtures on a protein basis. The bitterness of the samples from ALACENTM 392 was formally evaluated against two standard hydrolysates. The scores for bitterness on a scale of 1 to 10, 10 being most bitter were 1.9 for a sample after 0.5h hydrolysis, 2.3 for the 2h hydrolysis compared to 5 and 7 for the standard hydrolysis samples of greater degrees of hydrolysis.

25 The samples of ALACENTM 421 and a mixture of ALACENTM 392 and lactose taken after 2h had a mean particle size of 3µm or 2µm respectively. The sample of ALACENTM 392 had a mean particle size of 6µm after 2h hydrolysis and inactivation as specified. Less grittiness and chalkiness was attributed to the smaller particle size samples.

30

The solubility of the hydrolysed ALACENTM 392/lactose mixture was the highest with approximately 85% across the pH range. The ALACENTM 392, ALACENTM 421 samples are soluble to about 70% with a slight drop in solubility to 65% at pH 3.5.

35 Example 5

Three different solutions from ALACENTM 392, ALACENTM 421 and a mixture of ALACENTM 392 and lactose were made up of 30% solids to yield 75L. The enzyme

treatment was done using the same conditions as example 4. The samples taken at half hourly intervals were diluted to 15% solids. Otherwise the heat treatment was done as in example 4. The ACE-I activity measured as specified in example 1 was 0.560g/L, 0.440g/L and 0.728g/L.

5

Samples from example 4 and 5 were added in a concentration of 0.1% to the standard growth media of *Bifidobacterium lactis* and resulted in a faster cell growth and higher final cell density of the strain than the control without any supplement.

- 10 The oligosaccharide level (trisaccharides and higher) of those three hydrolysed samples was 0.2%, 2.1% and 7.0% in ALACENTM 392, ALACENTM 421 and the mixture of ALACENTM 392 and lactose, respectively.

Example 6

15

Hydrolysate powders prepared in example 5 were used as a supplement for yoghurts in addition rates from 2.5% and 5% of the final yoghurt and resulted in an increased creaminess and improved the texture compared to the control.

20

Example 7

The hydrolysate powders prepared in example 5 were used as the protein source in a muesli bar recipe on a 6% and 12% w/w addition rate. All tasters preferred the 5 hydrolysate bars over the unhydrolysed WPC control. The best results were achieved with hydrolysed ALACENTM 421 and a mixture of ALACENTM 392 and lactose prepared in example 5.

Example 8

10

The hydrolysate powder prepared in example 5 was used as an ingredient in a meal replacer concept sample. ALACENTM 421 hydrolysed in lactose and protein was added at a rate of 45% w/w to whole milk powder, malto dextrin, sucrose and milk calcium (ALAMINTM) to result in a powder meal replacer prototype. In comparison with a 15 control sample without hydrolysed whey protein, hydrolysed whey protein prepared in example 5 was found to be more acceptable.

Example 9

20 A nutritional whey protein drink was formulated containing 8% w/w of ALACENTM 392 or ALACENTM 421 or a mixture of ALACENTM 392 and lactose hydrolysed as specified in example 5. The drink also contained sucrose, citric acid, flavouring and colouring agents. The pH of the drink was adjusted to 4.3. The drink combined the nutritional and health advantages of whey protein with the refreshing taste of a soft drink. Compared 25 to a drink containing untreated whey protein control the pH stability was improved and the drink had a more milk like appearance than the control.

Example 10

30 A further nutritional protein drink was formulated containing 12.5% w/w of ALACENTM 421 hydrolysed as in example 5 in water mixed with pasteurised whole milk. Sucrose was added to yield 6% of the final formulation as well as stabiliser. The drink was flavoured when desired with banana, vanilla or similar flavours. To achieve an extended shelf life the drink was ultra high heated to 140°C for 3 seconds. The mean particle size 35 remains at 3 microns after the additional UHT heat treatment.

Example 11

The hydrolysis was carried out as specified in example 5 but instead of reconstituting ALACEN™ 421 powder a fresh retentate of ALACEN™ was concentrated to 5 30% solids in the solution. The neutrase addition rate was varied to 0.9% w/w (on a protein base), the lactase level as specified. The reaction mixture was inactivated at 15% solids after 2h. The ACE-I activity yielded 0.480g/L. The organoleptic properties, particle size and food application were very similar to example 4 and 5.

10 Example 12

The hydrolysis was carried out as specified in example 4 with ALACEN™ 421 powder. The Neutrase addition rate was varied to 0.9% w/w (on a protein basis). The lactose was converted with a lactase from *Aspergillus oryzae* (Fungal lactase 30,000, Kyowa 15 Enzymes Co. Ltd. Japan) on an addition rate of 0.4% w/w (on lactose base). The reaction mixture was inactivated after 1.5h with direct steam injection to achieve a temperature of 88°C for either 1.5 seconds or 3 seconds.

The particle size was 2.3 microns. Organoleptic properties and food application were 20 very similar to the product of example 4.

Example 13

A 10% w/w solution of ALACEN™ 392 was hydrolysed with a commercial protease 25 from *Bacillus subtilis* Neutrase (Novo, Nordisk Denmark) at an enzyme concentration of 0.9% w/w. The reaction continued for 6h at 50°C. Samples of 200ml were taken every 1h, inactivated at 88°C for 8 seconds and subsequently freeze dried.

ACE-I activity, degree of hydrolysis, pH of solution and bitterness developed over time 30 as follows. The higher the bitterness score the more bitter is the taste. The smaller the level measured, the higher is the ACE-I activity.

TABLE 1: Hydrolysis of ALACENTM 392 WPC

	Hydrolysis time [h]	ACE-I activity [g/L] (IC ₅₀)	Degree of hydrolysis [%]	pH of solution	Bitterness score [informal, 0- 10]
5	1	0.420	3.86	7.01	0
	2	0.280	3.78	6.96	1
	3	0.230	4.53	6.92	1
	4	0.220	4.89	6.89	3.5
	5	0.210	5.20	6.87	2
10	6	0.190	5.37	6.87	4.5

Example 14

- 15 A 10% w/w solution of ALACENTM 392 was hydrolysed with the following commercial proteases at 1% w/w, 50°C for 1h. The reaction was inactivated at 88°C for 8 seconds and subsequently the hydrolysate was freeze dried.

TABLE 2: Hydrolysis with Different Enzymes

Enzyme	ACE-I activity [g/L](IC ₅₀)	pH	Degree of hydrolysis [%]
5 Protease P6, neutral protease, <i>Aspergillus</i> strains, Amano Enzymes	0.274	7.0	8.9
Protease A, neutral protease, <i>Aspergillus oryzae</i> , Amano Enzymes	0.443	7.0	9.2
Protease M, acid protease, <i>Aspergillus oryzae</i> , Amano Enzymes	0.450	4.0	7.4
10 Peptidase, neutral peptidase, <i>Aspergillus oryzae</i> , Amano Enzymes	0.540	7.0	6.9
Neutrase, neutral bacterial protease, <i>Bacillus subtilis</i> , Novo Nordisk DK	0.510	7.0	4.3
15 Validase (Genancor), acid fungal protease, <i>Aspergillus niger</i> , Enzyme Services Ltd. NZ	0.510	4.0	5.6
AFP 2000 (Genancor), acid fungal protease, <i>Aspergillus niger</i> , Enzyme Services Ltd. NZ	0.550	4.0	3.9

20 Example 15

Identification of ACEI-Peptides and Measuring their Activities

200 mg of permeate from example 3 was dissolved in 0.1% trifluoroacetic acid (TFA) and applied to a Jupiter preparative reverse-phase HPLC column (10 micron, C18, 22 x 250 mm [Phenomenex NZ]) equilibrated with solvent A (0.1%TFA) and connected to an FPLC system (Pharmacia). Peptides were sequentially eluted from the column with a gradient of 0 to 43% solvent B (0.08% TFA in acetonitrile) in 245 min at a flow rate of 10mL/min. Peptides eluting from the column were detected by monitoring the absorbance of the eluate at 214nm. The eluate was collected by an automatic fraction collector set to collect 3 min fractions.

Each fraction was lyophilised and the amount of peptide material present was measured gravimetrically. Fractions were assayed for ACE-I activity using an *in vitro* assay system (reagents from Sigma product 305-10) consisting of rabbit lung ACE and the

colorimetric ACE substrate furylacryloylphenylalanylglycylglycine (FAPGG); ACE hydrolyses FAPGG to give the products FAP and GG which results in a decrease in absorbance at 340nm. If a peptide inhibits ACE, the change in absorbance at 340nm is reduced. Fractions containing the highest ACE inhibitory activity per mg peptide
5 material were re-applied to the preparative reverse-phase HPLC column and eluted using a shallow gradient of solvent B *i.e.* 0.09% increase in solvent B concentration/min. The eluate was collected using the fraction collector set to collect 0.5 min fractions.

Samples from each fraction were analysed using an analytical reverse-phase HPLC
10 column, and those fractions containing a single, identical peptide were pooled. Each pooled fraction was lyophilised and the weight of the peptide present was determined gravimetrically. The purified peptides were assayed for ACE-I activity as before and the IC_{50} was calculated for each individual peptide.

15 The molecular weight of each peptide was determined by Electrospray Ionisation Mass Spectrometry (Sciex API 300 triple quadrupole mass spectrometer). Tandem mass spectrometry was also done for each peptide to generate CAD spectra using MSMS experiment scans. Each peptide was also analysed by an automated N-terminal sequencer (ABI model 476A protein sequencer). Data collected from all three
20 techniques was used to deduce the sequence of all of the peptides possessing ACE-I activity. The origin of each of the active peptides was determined by searching a database containing the known sequences of all bovine milk proteins.

The peptides, their origins, activities and known similarities are set out in table 3.
25 Although the last three peptides are of a casein origin they were from a whey protein hydrolysate. The rennet used to precipitate casein did not precipitate these casein fractions and they remained with the whey proteins.

TABLE 3: ACE-I Peptides and their Activities

	Peptide Sequence ^a	Origin	Activity ^b (IC ₅₀ in mg L ⁻¹)	Similarity to known ACE-I Peptides
5	AFE (Ala-Phe-Glu)	PP ^d 3(129-131)	20	
	LFSH (Leu-Phe-Ser-His)	PP3(125-128)	30	
	ILKEKH (Ile-Leu-Lys-Glu-Lys-His)	PP3(71-76)	20	
10	LIVTQ (Leu-Ile-Val-Thr-Gln)	β -LG ^e (1-5)	17	
	MKG (Met-Lys-Gly)	β -LG(7-9)	24	
15	LDIQK ^c (Leu-Asp-Ile-Gln-Lys)	β -LG(10-14)	17	β -LG(9-14)
	VF (Val-Phe)	β -LG(81-82)	19	
	ALPMH (Ala-Leu-Pro-Met-His)	β -LG(142-146)	12	β -LG(142-148)
20	VTSTAV (Val-Thr-Ser-Thr-Ala-Val)	GMP ^f (59-64)	30	
	LHLPLP (Leu-His-Leu-Pro-Leu-Pro)	β -CN ^g (133-138)	7	
25	LVYFPFGPIPNLQNP (Leu-Val-Tyr-Pro-Phe-Pro- Gly-Pro-Ile-Pro-Asn-Ser- Leu-Pro-Gln-Asn-Ile-Pro- Pro)	β -CN(58-76)	19	β -CN(74-76)
30	LFRQ (Leu-Phe-Arg-Glu)	α _{s1} -CN(136-139)	17 ^h	

^a sequence given using the single-letter amino acid code with the corresponding three-letter code in brackets

^b using the colorimetric substrate FAPGG

^c most abundant ACE-I in hydrolysate

5 ^d protease peptone

^e β -lactoglobulin

^f glycomacropeptide

^g β -casein

^h activity measured with that of another peptide of unknown origin

10

Example 16

The effect of the hydrolysate powder prepared in example 3 (without ultrafiltration) on *in vivo* blood pressure was tested using spontaneously hypertensive rats (SHR/N). The
15 rat strain has been specifically selected for their development of high blood pressure on maturing, and is used extensively to monitor the effect of blood pressure lowering agents. They were purchased from Animal Resources Centre, P O Box 1180 Canning Vale, Western Australia 6155.

20 Eight week old rats were individually housed in plastic rat cages and kept in temperature controlled facilities throughout the trial. They had unlimited access to water and were fed commercial rat chow *ad libitum*. The test products were given orally as a single daily dose for 8 weeks during which time changes in blood pressure were monitored. Their blood pressure was measured using a specially designed tail cuff and blood
25 pressure monitoring apparatus (IITC Inc., Life Science Instruments, 23924 Victory Blvd, Woodland Hill, CA 91367). The experimental design was approved by the Massey University Animal Ethics Committee, protocol number 98/141.

The changes in the systolic blood pressures of each group of animals over the eight
30 weeks are plotted in Figure 2 (as least squares means). The hydrolysate at both 2g/Kg bodyweight/day and 4g/Kg bodyweight/day significantly lowered the systolic blood pressure of SHRs compared to animals fed commercial rat chow only ($p < 0.004$ by least-squares means analysis, see Figure 3). The effect of the hydrolysate was not as great as that of captopril, a known ACE-I inhibitory drug administered at 30mg/Kg
35 bodyweight/day, but was a significant improvement for animals fed commercial rat chow only.

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CLAIMS

1. A process for preparing a soluble whey protein hydrolysate containing bioactive peptides comprising hydrolysing a whey protein-containing substrate with one or more enzymes characterised in that
- 5
- i) the enzyme is a heat labile protease,
- ii) the hydrolysis is conducted at a temperature of between about 30°C and 70°C at a pH of about 6 to about 8.5 when said enzymes is a neutral proteases, and at a pH of about 3.5 to about 5 when said enzyme is an acid
- 10
- protease and 3.5 to 5.0 where said enzyme is an acid protease,
- iii) the hydrolysis is terminated when a degree of hydrolysis of no greater than 15% has been reached,
- iv) the hydrolysis is terminated by deactivating said one or more enzymes, and
- v) the conditions for said step iv) are sufficiently mild to avoid substantial
- 15
- denaturation peptides in said hydrolysate.
2. A process as claimed in claim 1 wherein said substrate is sweet whey or sweet whey protein concentrate.
- 20
3. A process as claimed in claim 1 or 2 wherein said enzyme is selected from the group consisting of Protease P6, Protease A, Protease M, Peptidase, Neutrase, Validase and AFP 2000 (all as herein defined).
4. A process as claimed in claim 1, 2 or 3 wherein said enzyme deactivating step iv) comprises heat deactivation.
- 25
5. A process according to claim 4 wherein said heat deactivation comprises heating and hydrolysate for up to ten seconds to a temperature up to 95°C.
- 30
6. A process according to claim 4 wherein said hydrolysis has been conducted at a temperature of below 65°C, wherein said heat deactivating step is conducted at 65°C to 70°C for from 10 seconds to 15 minutes.
7. A process according to claim 4 wherein said hydrolysis has been conducted at a
- 35
- temperature below 60°C, wherein said heat deactivating step is conducted at 60° to 65°C for from 10 seconds up to 30 minutes.

8. A process as claimed in claim 1, 2 or 3 wherein said enzyme deactivating step comprises altering the pH of said whey protein-containing substrate to a pH at which said protease is not active.
- 5 9. A process as claimed in claim 8 wherein said enzyme deactivating step includes heat deactivation as claimed in any one of claims 4 to 7.
10. A process as claimed in claim 1, 2 or 3 wherein said enzyme deactivating step iv) comprises subjecting said hydrolysate to ultrafiltration with an ultrafiltration
10 membrane having a nominal molecular weight cutoff in the range of 10-500kDa.
11. A process as claimed in any one of the preceding claims wherein said enzyme is immobilised on an inert support during said hydrolysis step ii).
- 15 12. A process as claimed in claim 11 wherein said inert support is Roehm Eupergit, carrageenan particles, chitosan particles or any other suitable inert support material.
13. A process as claimed in any one of the preceding claims wherein the degree of
20 hydrolysis is about 3-5%.
14. A process as claimed in any one of the preceding claims wherein the substrate also contains lactose, in an amount of about 5% by weight or higher.
- 25 15. A process as claimed in any one of the preceding claims wherein said lactose content is about 10% by weight or higher.
16. A process as claimed in claim 14 or 15 wherein the amount of lactose present in the substrate is up to about 30% by weight.
- 30 17. A process as claimed in claim 14 or 15 wherein the amount of lactose present in the substrate is up to about 50% by weight.
- 35 18. A process as claimed in any one of claims 14 to 17, wherein the substrate is also treated with lactase and/or β -galactosidase, either before, during or after the whey protein hydrolysis, to hydrolyse the lactose to galactose and glucose and synthesize galacto-oligosaccharides.

19. A process as claimed in any one of the preceding claims wherein the hydrolysate so prepared contains one or more of the bioactive peptides selected from the group consisting of AFE, LFSH, ILKEKH, LIVTQ, MKG, LDIQK, VF, ALPMH, VTSTAV, LHLPLP, LVYFPFGPIPNLSLPQNIPP and LFRQ.
- 5 20. A non-bitter soluble whey protein hydrolysate produced by a process according to any one of claims 1 to 19.
- 10 21. A product as claimed in claim 20 wherein the degree of hydrolysis of the whey proteins is about 3 to 5%.
22. A product as claimed in either of claims 20 or 21 wherein the mean particle size of the whey proteins in the product is less than about 30 microns.
- 15 23. A product as claimed in claim 22 wherein said mean particle size is less than about 3 microns.
24. A product as claimed in any one of claims 20 to 23 which is substantially white in appearance.
- 20 25. A product as claimed in any one of claims 20 to 24 which also contains galacto-oligosaccharides.
- 25 26. A product as claimed in any one of claims 20 to 25 wherein one or more of said bioactive peptides is selected from the group consisting of AFE, LFSH, ILKEKH, LIVTQ, MKG, LDIQK, VF, ALPMH, VTSTAV, LHLPLP, LVYFPFGPIPNLSLPQNIPP and LFRQ.
- 30 27. A food product containing a whey protein hydrolysate as claimed in any one of claims 20 to 26.
28. Any one or any combination of two or more of the bioactive peptides selected from the group consisting of AFE, LFSH, ILKEKH, LIVTQ, MKG, LDIQK, VF, ALPMH, VTSTAV, LHLPLP, LVYFPFGPIPNLSLPQNIPP and LFRQ.
- 35 29. A method of reducing systolic blood pressure in a subject which comprises administering to that subject an effective amount of a product as claimed in any one of claims 20 to 28.

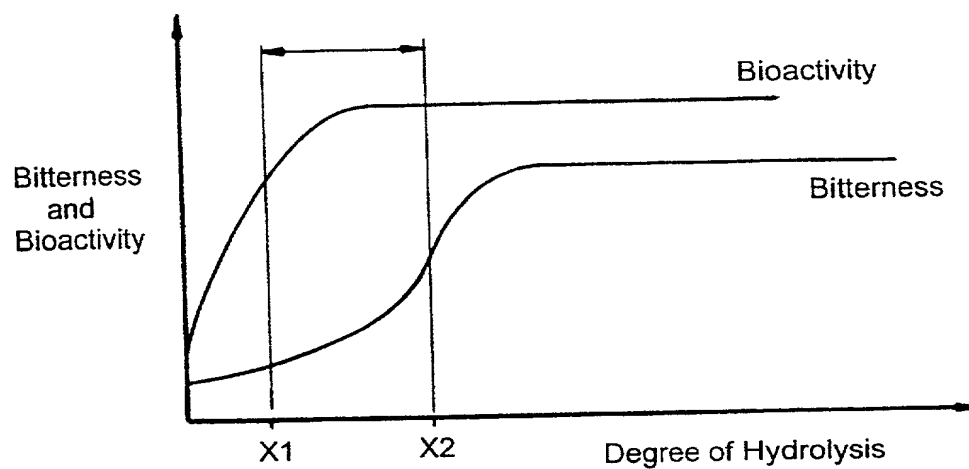
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30. A method as claimed in claim 29 which comprises administering an effective amount of a product according to claim 26.
31. A method as claimed in claim 29 which comprises administering an effective amount of a peptide or a combination of peptides as claimed in claim 28.
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**FIG. 1**

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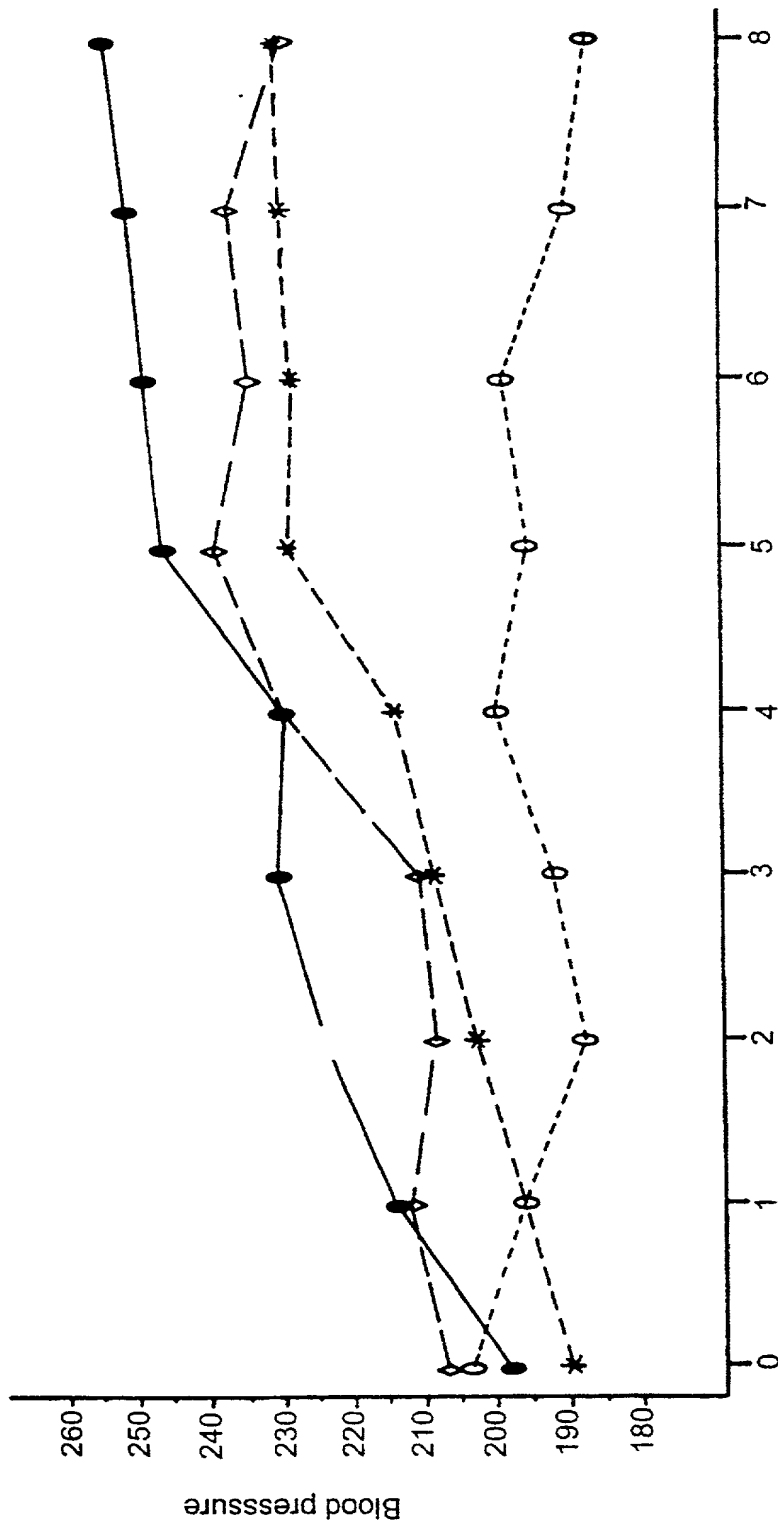
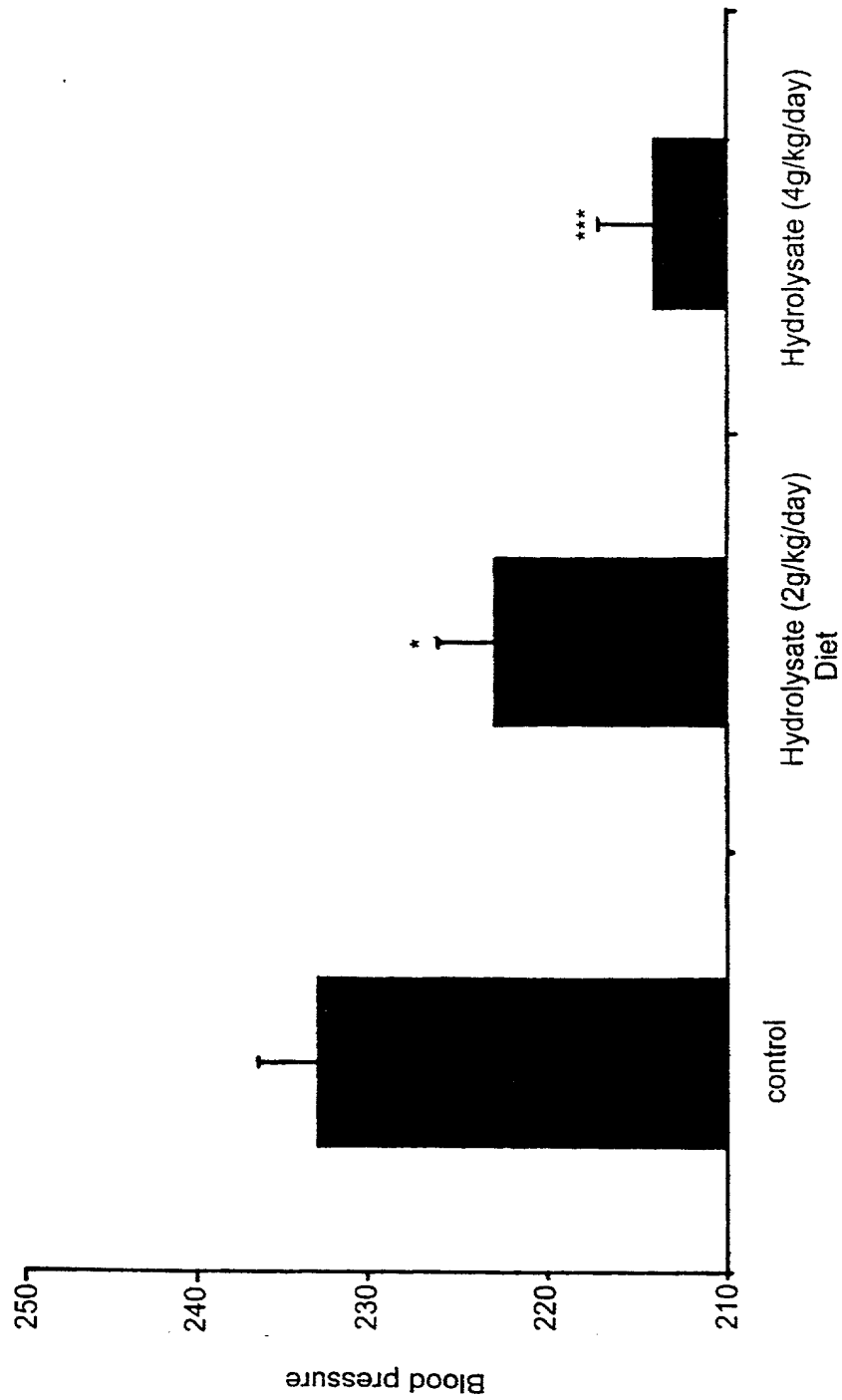


FIG. 2

Control ●-●-●
 Hydralysate (2g/kg bodyweight/day) ○-○-○
 Hydralysate (4g/kg bodyweight/day) *-*-*
 Captopril (30mg/kg bodyweight/day) ○-○-○

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* $p=0.048$ *** $p=0.0006$ **FIG. 3**

DECLARATION - USA PATENT APPLICATION

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name;

I believe I am an original, first and joint inventor of the subject matter which is claimed and for which a patent is sought on the invention entitled BIOACTIVE WHEY PROTEIN HYDROLYSATE; the specification of which was internationally filed on **June 14, 1999** as Application Serial No. **PCT/NZ99/00084**, and now filed in the United States as Application Serial No. **09/720,041**, filed on **December 14, 2000**.

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above;

I acknowledge the duty to disclose information which is material to patentability as defined in Title 37, Code of Federal Regulations, § 1.56;

I hereby claim foreign priority benefits under Title 35, United States Code, § 119(a)-(d) of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

PRIOR FOREIGN APPLICATION(S)

Priority
Claimed

No.: **330710**

Country: **New Zealand** Date Filed: **June 17, 1998**

Yes

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful, false statements may jeopardize the validity of the application or any patent issued thereon.

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